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Cracking of Waste Engine Oil in Presence of Cobalt Oxalate

Abstract

Nowadays, demand for lube oil is increasing because of increased use of vehicles. This increased use of lube oil is generating almost 60% of waste engine oil. It is estimated that worldwide over 25 million tons waste engine oil is generated annually worldwide. Waste lube oil consists of various organic compounds other than hydrocarbons; it contains solvent, heavy metals, combustion products etc.lf not disposed off carefully these components harm the environment and are very difficult to get rid of these components (e.g. soot, Poly-cyclic aromatic hydrocarbons (PAHs). Generally, to get rid of waste oil, simple methods of Incineration and Combustion for Energy Recovery and Vacuum Distillation and Hydro-Treatment for Re-Refining are practised. However, these methods can only get rid of the chemical value of waste and they become increasingly impracticable because of concerns over environmental pollution due to combustion products. These processes even involved difficulties and additional costs of sludge disposal, recognized due to the undesirable contaminants present in waste oil. Catalytic Cracking is the unique environment friendly technique to get rid of waste lube oil. Temperature, pressure, reactor type, type of material is having direct effect on catalytic cracking which results differently to form hydrocarbon oils, gases and coke. Oil and gas are the end products having high calorific value. Advantage of catalytic cracking process is gaining 86% oil, 10% gas, rest is residue. The study of catalytic cracking technique is done to explore yield (product quantity, qualification of catalytic cracking of oil, especially Hydrocarbon composition using cobalt oxalate as a catalyst) to the benefits of society and industry. Indeed, this technique can reduce costs from imported technology and produce alternative choice of energy from wastelube oil and thereby reduce the imports of crude oil.

Keywords: Waste Engine Oil, Cracking, Combustion Products, Degradation Products, Petrochemicals, ASTM, ^OAPI, Waste to Energy, Recycling Waste, Cracking.

Introduction

The study of catalytic cracking of waste engine oil is done to explore yield of valuable products (product quantity,qualification of catalytic cracking of oil, especially Hydrocarbon composition using cobalt oxalate as a catalyst) to the benefits of society and industry.

Objective of this work is conservation of precious resource and environment protection. Little reduction in imports of high value oil can result in saving valuable foreign exchange.Efforts for regeneration or converting this waste/used oil to valuable petroleum products can result in making it a highly valuable resource.

Therefore it can be said that, used oil, a valuable resource, is wasted if improperly disposed off.Conserving and utilizing it more effectively means directly boosting country's energy resources.Immediate effect of such conservation can be small but effective reduction in energy imports as our country is almost totally dependent on crude oil / lube base oil imports.All these efforts can result in saving of huge amount of foreign exchange and utilizing better the countries financial resources.

When used oil is dumped, it is capable of seeping into ground and surface water.Just one liter of used oil can render one million liters of water undrinkable.It is also a serious threat to plant and animal life.Marine species can be adversely affected by oil concentrations as low as one ppm. Loss of plants and animal life, while tragic, also results in economic loss.When used oil is burnt, it results in the incomplete combustion, thus increasing the air pollution. Hence, re-refining or converting used oil to other valuable products is much better option over burning or other means

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of disposal or re-use. And thus checks environmental degradation and saves ecology.

Experimental Procedure

In this study, waste engine oil was collected from different private two wheeler service stations in Amravati city and mixed together to form a single homogeneous sample. Table-1

Properties of Filtered and Dehydrated Waste Oil

S.N.	Property	Observations	
		a) at 40 °C - 424	
1.	Redwood Viscosity	seconds.	
		b) at 100 °C -61	
		seconds.	
2.	Specific Gravity at 29 °C	0.8885	
3.	API Gravity at 29 °C	0	
э.	ATT Glavity at 29 C	27.7589 API	
4.	Pour Point	-24 °C	
5.	Flash Point (Clevland	193 °C	
	Open Cup method)		
6.	Fire Point (Clevland	252 °C	
	Open Cup method)		
7.	Conradson Carbon	0.9088%	
	Residue (wt %)		
	Cobalt-based catalyst	ts are important i	

Cobalt-based catalysts are important in reactions involving carbon monoxide; steam reforming also uses cobalt oxide-base catalysts. Use of cobalt oxalate in gasification of hydrocarbon stocks is well established. Cobalt is also a catalyst in the Fischer Tropsch process. The hydrodesulphurization of petroleum uses a catalyst derived from cobalt and molybdenum. The hydroformylation of alkenes often rely on cobalt octa-carbonyl as the catalyst, although such processes have been partially displaced by more efficient iridium- and rhodium-based catalysts. Therefore cobalt based catalysts i.e. Cobalt Oxalate [CoC_2O_4] is considered for the cracking of waste engine oil.

A 3 liters batch reactor prepared for this purpose is used to perform the experiment, which is of 90 mm height and 206 mm diameter.

1200ml (1090.5gms) of feed is cracked in the batch reactor at 420°C in presence of 1.0% cobalt oxalate. At 394°C vapors starts coming out of the reactor indicating the start of cracking reactions. The temperature of the reactor is immediately raised and maintained at 420°C as closely as possible. 939.7gms of distillate (cracked product) is collected and 40.89gms of residue is obtained from the experiment. Total material balance on reactor indicates that 109.92gms of feed is gasified; 939.7gms of liquid products are obtained while 40.89gms of residue is formed.

Tab	le-2
Motorial	Delenee

S. N.	Products	Products Obtained, Gms	% Products Obtained
1.	Liquid product obtained, (gms)	939.7	86.17
2.	Residue formed, (gms)	40.89	03.75
3.	Feed gasified, (gms)	109.92	10.08

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4.	Total amount of product formed (liquid+gases), gms	1049.62	96.25
5.	Time required to start liquid collection, (mins)	43	
6.	Time required from 400°C to completion of cracking, (mins)	49.00	
7.	Total time required for cracking, (mins)	93	

Table-3

Properties of Products Obtained

S.N.	Properties	Observations
1.	Redwood viscosity, seconds, at 40°C	43
2.	Specific gravity,at 29°C	0.8409
3.	API Gravity, °API at 29°C	36.7721
4.	Aniline point,°C	77.5
5.	Flash point (Clevland open cup method),°C	39
6.	Fire point (Clevland open cup method), °C	56
7.	Conradson carbon residue, wt%	0.0195
8.	Pour point, °C	-13
9.	Bromine number	3.83
10.	Acid value, mg KOH/gm	0.5991

Liquid products obtained are subjected to various tests such as Distillation characteristics (IP123/93), Redwood viscosity (IP70/62 25th edition), Specific gravity (API Gravity), Aniline Point (IP2/91, ASTM D611-87, ISO 2977:1989(E)), Conradson Carbon Residue (CCR) (IP13/82,ASTM D189-88, BS: 2000 Part 13:1993), Pour Point (IP15/67, ASTM D 97-87, BS:2000:Part 15:1993), Flash and Fire Point by Clevland Open Cup Method (IP 36/84(1989), ASTM D92-90)), Total Acidity (IP 1/74 (1990), BS 2000: Part 1:1993)) Bromine Number (IP129/93, BS2000 : Part 129:1993) etc. (19,20)

The gaseous products obtained can be a very good feedstock for petrochemicals or can be used as a fuel in the industry. ASTM distillation characteristics of the product obtained from this experiment shows that around 12.5%(vol.) material falls in the gasoline range (<200°C), 62.5%(vol.) material falls in the gas oil range (200-390°C) i.e. dieseland around 22.5% (vol.) material boils in the range of 390°C-408°C. While 0.75% residue collected from distillation flask; 1.75% vapor losses occurred during the distillation. Details of the ASTM distillation characteristics of liquid products obtained are shown in Table-4.

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Table-4 ASTM Distillation Characteristics of Distillate Obtained

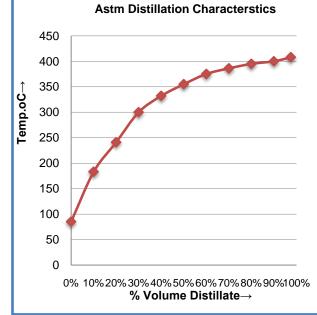
S.N.	Time (mins.)	Temp. °C	% Volume Distillate	Observations
1.	00	40		Heating Started
2.	25	85		I.B.P.
3.	55	183	10	Foaming Observed
4.	65	241	20	
5.	72	300	30	
6.	74	332	40	
7.	76.5	355	50	
8.	79	375	60	
9.	81	386	70	
10.	83	395	80	
11.	85	400	90	
12.	88	408	97.5	Final Boiling Point
Total Distillate Collected: 97.50%, Residue:				
0.750/ 1.555.00 1.750/				

0.75%, Losses: -- 1.75%.

Figure-1

ASTM Distillation Characteristics

of Distillate Obtained



Aim of the Study

Objective of this work is conservation of precious energy resource and environment protection. **Conclusion**

The catalytic cracking of waste engine oil at 420°C in presence of 1.0% cobalt oxalate yields 10.08% (wt) hydrocarbon gases, 86.17% (wt) liquid products and 3.75% (wt) residue. The viscosity, specific gravity/API gravity, flash point and fire point of products indicates the extent of cracking occurred. As all the contaminants accumulate in residue, the liquid and gaseous products obtained are free from all type of contaminants that makes these products as clean as virgin fractions obtained in the refinery. So these products forms high value refinery streams, 62.5% products can be blended with diesel fraction and 12.5% products are suitable to blend in gasoline range product.

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It should be noted that the problems related to used oil treatments either by vacuum distillation (such as fouling of heating and distillation equipment), or by using it as a fuel in cement kilns, furnaces etc. which have potential to cause serious harms to the environmentcan be avoided by catalytic cracking of these oils in presence of cobalt oxalate.

This can be one of the ways to conserve the valuable oil and reducing the rate of depletion of crude oil. So used lubricating oil may again be a source of fuels. Recycling doesn't just slow the depletion of number one resource; it also saves energy and reduces the pollutions of land, water and air. Mismanagement of waste lube oil is a serious environmental as well as economical problem. Almost all types of waste oil have the potential to be recycled safely, saving a precious non-renewable source and at the same time minimizing environmental pollution. Besides its great adverse impact on the environment, if used oil is properly recycled and/or reused, it could have significant savings on fresh crude oil. Disposal of used lubricating oil into the eco-system creates environmental hazards. Tough laws are being enacted throughout the world for the disposal of waste petroleum products and every genuine effort should be made for its re-use.

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